

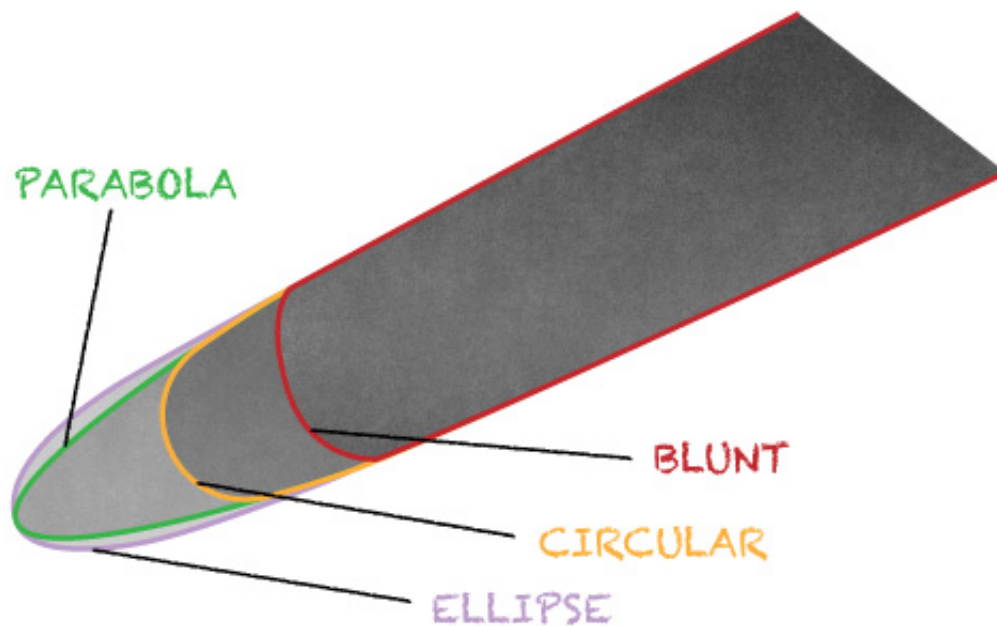
Here are some brief reminders about $NPSH_A$ and $NPSH_R$.

NPSH changes with:

Impeller diameter: For the same flowrate on a given system an impeller of a smaller diameter will have a higher $NPSH_R$.

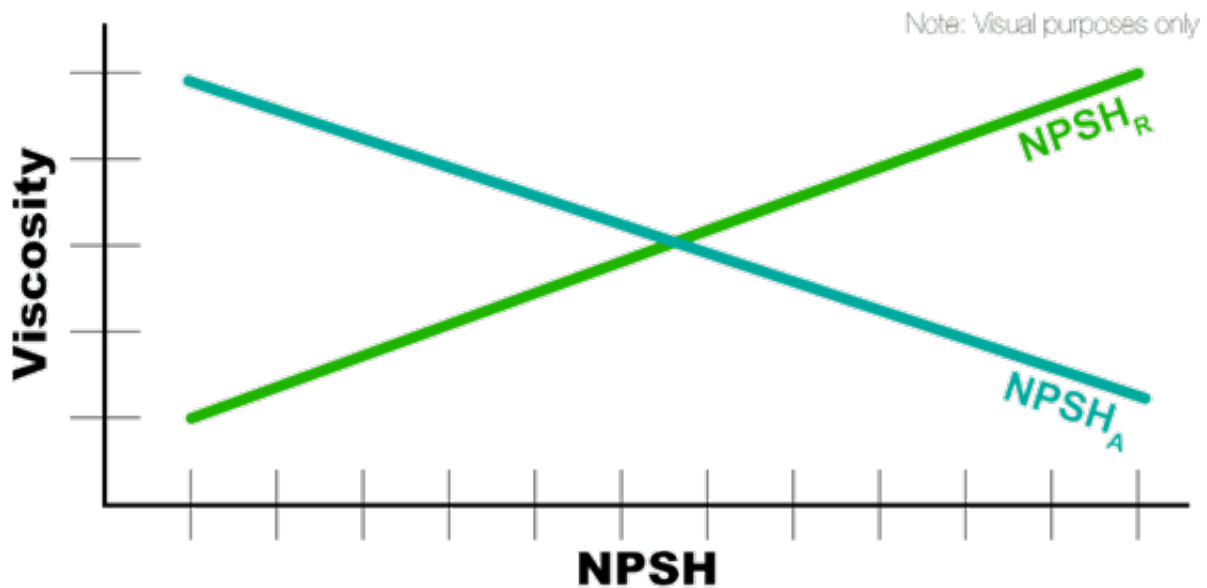
Clearance of impeller and wear rings: As clearances open up on the pump over time the $NPSH_R$ will also increase. This effect is significantly worse for closed impellers than open or semi open styles.

Vane geometry: Specifically the leading edge profile of impeller vanes. The shape of the leading edge will affect $NPSH_R$. Vane geometry in order of best shape to worse shape are 1) parabola 2) ellipse 3) circular 4) blunt.



Speed: Not always 100% true, but for small speed changes $NPSH_R$ will vary approximately as the square of the speed ratio for the pump in the midrange operating region and near BEP. For sure, $NPSH_R$ increases with speed and vice versa.

Viscosity: Yes an increase in viscosity will increase the $NPSH_R$ and decrease the $NPSH_A$. There must be a correction for viscous fluids. In one simple word ... friction. See note at bottom for more info.



Air Entrainment: Air entrainment in a range of 0.3 to 1.0 percent will actually

work to help the NPSH issues, but above 1% the $NPSH_R$ will increase.

Age of system and pump (fouling and corrosion): As systems age and or foul the flow velocity profile and the friction increase. Both factors work to reduce $NPSH_A$ and increase $NPSH_R$.

Suction pipe geometry: For every elbow, twist and turn in the suction pipe the fluid velocity profile becomes turbulent (technical for; it gets all messed up) and creates a mismatch (discrepancy) between the fluid velocity and the impeller inlet vane velocity. This mismatch creates recirculation at the impeller eye that directly affects $NPSH_R$.



NPSH Margins: Last; please understand that pumps with adequate NPSH (calculated) margins...where $NPSH_A$ exceeds $NPSH_R$ can still cavitate, because the margins are not sufficient and the system dynamics are changing.



Quiz: On your own...see if you understand why the following factors affect NPSH.

1. Temperature both ambient and fluid
2. Vapor Pressure
3. Specific Gravity of the fluid
4. Elevation above sea level

Bonus Info:

Pumps require a certain amount of Net Positive Suction Head (NPSH) to operate satisfactorily at a given point of head and flow on the curve to prevent cavitation. These points are empirically determined by the manufacturer (sometimes calculated) and are denoted as Net Positive Suction Head Required (NPSH_R).

The suction side of the system itself must in return provide a certain amount of NPSH and that is referred to as Net Positive Suction Head Available (NPSH_A). There must be more NPSH_A than NPSH_R for the pump to operate satisfactorily. The difference is referred to as the margin or ratio.

$$\text{NPSH}_A \div \text{NPSH}_R = \text{MARGIN RATIO}$$
$$\text{NPSH}_A - \text{NPSH}_R = \text{MARGIN}$$

Refer to Hydraulic Institute **9.6.1-2017** for details on margins and ratios.

Viscosity: ANSI/HI Standard **9.6.7- 2015** provides updated instructions for correcting a known water performance into an estimated viscous performance for a given viscosity.

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